

## Methyl orange as corrosion inhibitor for carbon steel in well water

J Sathiyabama, Susai Rajendran\*, J Arockia Selvi & A John Amalraj<sup>1</sup>

Corrosion Research Centre, Department of Chemistry, GTN Arts College, Dindigul 624 005, India

<sup>1</sup>Department of Chemistry, Loyola College, Chennai, India

Email: srmjoany@sify.com

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The corrosion inhibition efficiency of methyl orange in controlling corrosion of carbon steel immersed in well water has been evaluated by weight loss method both in absence and presence of zinc ion. A synergistic effect exists between methyl orange (MO) and  $Zn^{2+}$ . The inhibition efficiency (IE) of the MO –  $Zn^{2+}$  system decreases with increase in immersion period. Polarization study suggests that the MO- $Zn^{2+}$  system functions as a mixed inhibitor system. FTIR spectra indicate that the protective film consists of  $Fe^{2+}$  - MO complex and  $Zn(OH)_2$ .

**Keywords:** Carbon steel, Corrosion inhibition, Methyl orange, Zinc ion

Several compounds such as nitrite<sup>1,2</sup>, phosphates<sup>3,4</sup>, silicates<sup>5</sup>, sodium salicylate<sup>6</sup>, sodium cinnamate<sup>7</sup>, molybdate<sup>8,9</sup>, phosphonic acids<sup>10,11</sup>, polyacrylamide<sup>13</sup> and caffeine<sup>14,15</sup> have been used as corrosion inhibitors. Talati and Gandhi<sup>16-18</sup> have studied the effect of some dyes as corrosion inhibitors for B26S aluminium in hydrochloric acid. The inhibition efficiency (IE) of triphenylmethane dyes such as victoria blue, fast green, light green, malachite green, fuchsine base, fuchsine acid, crystal violet and methyl violet 6B in controlling corrosion of aluminium in phosphoric acid has been studied by Talati and Daraji<sup>19</sup> using weight loss and polarization studies. Corrosion inhibition of mild steel in acidic media by some organic dyes have been investigated<sup>20</sup>. Oguzie<sup>21</sup> has studied the inhibition of corrosion of mild steel in hydrochloric acid solution by methylene blue dye. Eriochrome Black-T serves as a good corrosion inhibitor for carbon steel in well water<sup>22</sup>. At pH 11 methyl orange along with  $Zn^{2+}$  functions as a good inhibitor in controlling corrosion of aluminium<sup>23</sup>. Dyes have chromophores and auxochromes. They can form films on metal surfaces by coordination through azo groups and/or  $\pi$  electrons of aromatic rings. Though several dyes have been used as corrosion inhibitors, the mechanistic aspects of corrosion inhibition have not been studied in detail. Present study was aimed to investigate (i) the inhibition efficiency of methyl orange (MO) in controlling the corrosion of carbon steel immersed in well water in the absence and presence of zinc ion, (ii) the influence

of pH and immersion period (iii) to analyze the protective film formed on the metal surface by FTIR spectroscopy (iv) to propose a suitable mechanism of corrosion inhibition based on the results of electrochemical study such as polarization and FTIR spectra.

### Experimental Procedure

#### Preparation of specimens

Carbon steel specimens (S, 0.0267; P, 0.067; Mn, 0.4; C, 0.1% and the rest iron), of the dimensions 1.0×4.0×0.2 cm were polished to mirror finish, degreased with trichloroethylene and used for weight loss method and surface examination studies.

#### Weight loss method

Relevant data of the well water used in this study are given in Table 1. Carbon steel specimens, in triplicate, were immersed in 100 mL of the well water and various concentrations of methyl orange in the presence and absence of  $Zn^{2+}$  (as  $ZnSO_4 \cdot 7H_2O$ ) for a period of one day. The corrosion products were cleaned with Clarke's solution<sup>24</sup>. The weight of the specimens before and after immersion was determined using Shimadzu balance AY62. The corrosion inhibition efficiency was calculated using Eq. (1)

$$IE = 100 (1 - W_2 / W_1) \% \quad \dots (1)$$

where  $W_1$  is the corrosion rate in the absence of inhibitor and  $W_2$  is the corrosion rate in presence of inhibitor.

### FTIR spectra

The structure of methyl orange is shown in Fig. 1. The carbon steel specimens immersed in various test solutions for one day were taken out and dried. The film formed on the metal surface was carefully removed and thoroughly mixed with KBr, so as to make it uniform throughout. The FTIR spectra were recorded in a Perkin–Elmer–1600 spectrophotometer.

### Potential dynamic polarization study

Polarization study was carried out in electrochemical impedance analyzer model CHI 660A, using a three electrode cell assembly; *iR* compensation was made. Carbon steel was used as working electrode with platinum as counter electrode and saturated calomel electrode (SCE) as reference electrode. The corrosion parameters such as corrosion potential ( $E_{\text{corr}}$ ), corrosion current ( $I_{\text{corr}}$ ) and Tafel slopes (anodic slope,  $b_a$  and cathodic slope,  $b_c$ ) were calculated.

## Results and Discussion

### Weight loss study

The corrosion inhibition efficiencies (IE) of methyl orange in controlling the corrosion of carbon steel immersed in well water, both in the absence and presence of zinc ion have been tabulated in Table 2. The values indicate that the ability of methyl orange

as a good corrosion inhibitor is enhanced significantly in presence of  $\text{Zn}^{2+}$ .

### Influence of immersion period on inhibition efficiency

The IE of 100 ppm MO-50 ppm  $\text{Zn}^{2+}$  system (Table 3) is found to decrease as the immersion period increases. This indicates that the protective film formed on the metal surface is unable to withstand the continuous attack of corrosive ions such as  $\text{Cl}^-$  ion (665 ppm) present in well water. There is a competition between the formations of  $\text{FeCl}_2$  (and also  $\text{FeCl}_3$ ) and Fe–MO complex (on the anodic sites of the metal surface). A perusal of the results suggests that the formation of  $\text{FeCl}_2$  is favoured when compared with the formation of Fe–MO complex<sup>25,26</sup>. Similar observations have been made by Selvaraj *et al.*<sup>25</sup>, while studying corrosion inhibition, using polyvinyl pyrrolidone and also by Rajendran *et al.*<sup>26</sup>, while investigating corrosion inhibition by sodium dodecyl sulphate.

### Influence of pH on inhibition efficiency

The IE of the MO– $\text{Zn}^{2+}$  system has been evaluated at different pH values of the solutions. IE values have been tabulated in Table 4. At pH 6 the IE is found to be 64%. This decrease in IE is due to the fact that the protective film formed on the metal surface is broken by the attack of  $\text{H}^+$  ions. At pH 8 the IE is 98%. Further increase in pH of the solution lowers IE substantially. Experimental results suggest that the amount of  $\text{Zn}^{2+}$  available to transport MO towards the metal surface decreases at high pH. This may be due

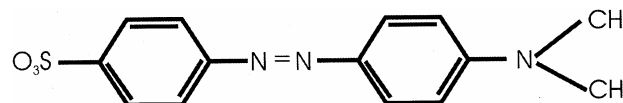


Fig. 1—Structure of methyl orange

Table 1—Parameters of well water

Parameter	Value
pH	8.38
Conductivity	3110 $\mu\text{mhos} / \text{cm}$
TDS	2013 ppm
Chloride	665 ppm
Sulphate	14 ppm
Total hardness	1100 ppm

Table 2—Corrosion rates (CR) of carbon steel in well water in the absence and presence of inhibitor and the inhibition efficiencies obtained by weight loss method.

MO (ppm)	Inhibitor system : Methyl orange (MO) + $\text{Zn}^{2+}$				Immersion period : One day			
	$\text{Zn}^{2+} = 0$ (ppm)		$\text{Zn}^{2+} = 10$ (ppm)		$\text{Zn}^{2+} = 25$ (ppm)		$\text{Zn}^{2+} = 50$ (ppm)	
	CR (mdd)	IE (%)	CR (mdd)	IE (%)	CR (mdd)	IE (%)	CR (mdd)	IE (%)
0	59.09	--	56.14	5	50.23	15	46.09	22
20	78.17	-32	1.185	96	10.05	83	4.14	93
60	69.08	-17	1.174	98	9.45	84	2.95	95
100	58.19	2	1.168	98	5.32	91	1.183	98
140	55.46	6	1.159	98	4.73	92	1.182	98
180	51.82	12	1.153	98	2.36	96	1.181	98

Table 3—Influence of immersion period on the inhibition efficiency of the MO – Zn<sup>2+</sup> system

Immersion period (day)	System		
	Well water	Well water + MO (100 ppm) + Zn <sup>2+</sup> (50 ppm)	
	CR (mdd)	CR (mdd)	IE (%)
1	59.09	1.18	98
3	21.52	0.86	96
5	14.9	1.94	87
7	17.0	2.89	83

Table 4—Influence of various pH on the inhibition efficiency of MO– Zn<sup>2+</sup> system

pH	System		
	Well water	Well water + MO (100 ppm) + Zn <sup>2+</sup> (50 ppm)	
	CR (mdd)	CR (mdd)	IE (%)
6	17.27	6.22	64
8	59.09	1.18	98
11	3.64	0.51	86

to the fact that zinc ions in the bulk of the solution are precipitated as zinc hydroxide.

#### Analysis of polarization curves

The potentiodynamic polarization curves of carbon steel immersed in well water in the absence and presence of inhibitors are shown in Fig. 2. The corrosion parameters are given in Table 5. When carbon steel was immersed in well water the corrosion potential was -550 mV versus SCE. The corrosion current was  $52.480 \times 10^{-5}$  A/cm<sup>2</sup>. When MO (100 ppm) and Zn<sup>2+</sup> (50 ppm) were added to the above system, the corrosion potential shifted to -557 mV versus SCE. The equal tafel slopes ( $b_a$  and  $b_c$ ) indicate that the formulation consisting of MO and Zn<sup>2+</sup> functions as a mixed inhibitor. In the presence of this inhibitor system, the corrosion current decreased from  $52.480 \times 10^{-5}$  to  $2.5118 \times 10^{-5}$  A/cm<sup>2</sup>. This suggests the inhibitive nature of this inhibitor system.

#### Analysis of FTIR spectra

The FTIR spectra of pure methyl orange and the MO-Fe<sup>2+</sup> (prepared by mixing MO and freshly prepared FeSO<sub>4</sub> and dried) are shown in Fig. 3a and 3b, respectively. Analysis of the two spectra shows that there is shift in -S=O symmetric stretching frequency from 1120 to 1111 cm<sup>-1</sup>; the -N=N- shifts from 1421 to 1383 cm<sup>-1</sup>. The aromatic C=C ring stretching frequency shifts from 1608 to 1641 cm<sup>-1</sup> and C-N stretching frequency shifts from 1367 to

Table 5—Corrosion parameters of carbon steel immersed in well water in the presence and absence of inhibitors

Inhibitor : MO (100 ppm) + Zn <sup>2+</sup> (50 ppm)					
MO (ppm)	Zn <sup>2+</sup> (ppm)	$E_{corr}$ (mV) vs SCE	$b_a$ (mV)	$b_c$ (mV)	$I_{corr}$ (A/cm <sup>2</sup> )
0	0	-550	115	125	$52.480 \times 10^{-5}$
100	0	-553	139	60.7	$3.3597 \times 10^{-5}$
100	50	-557	64	64	$2.5118 \times 10^{-5}$

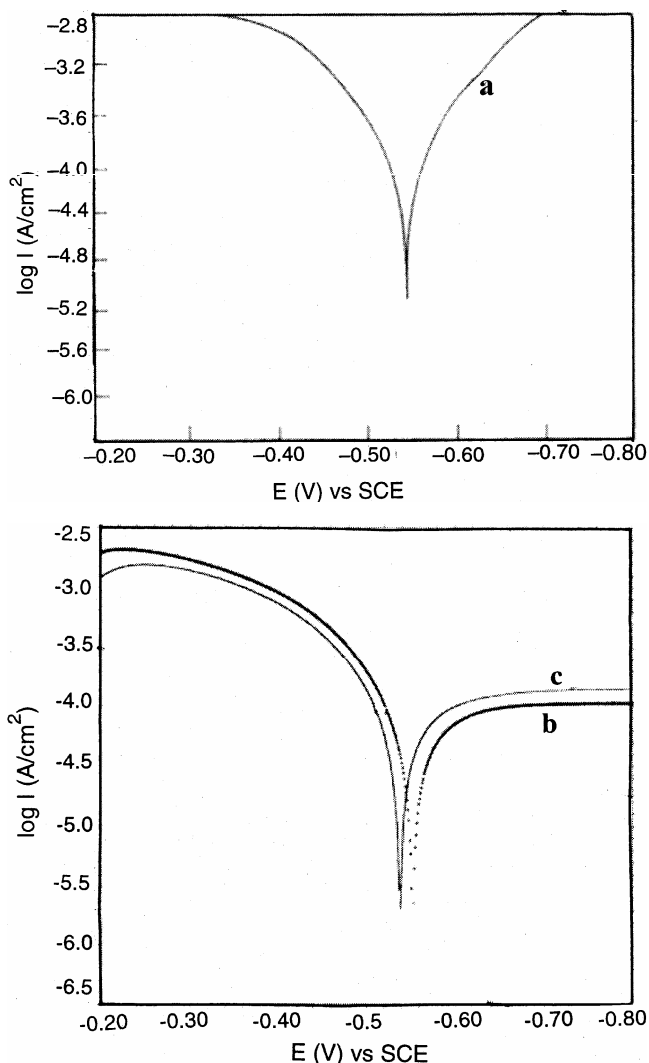


Fig. 2—Polarization curves of carbon steel immersed in test solution. (a) well water, (b) well water + MO (100 ppm), and (c) well water + MO (100 ppm) + Zn<sup>2+</sup> (50 ppm)

1383 cm<sup>-1</sup>. These observations suggest that MO forms complex with Fe<sup>2+</sup> by co-ordinating through oxygen atom of the sulphonic acid group, nitrogen atom of the azo group, the aromatic pi electrons and the nitrogen atom of the -N(CH<sub>3</sub>)<sub>2</sub> in methyl orange<sup>27</sup>.

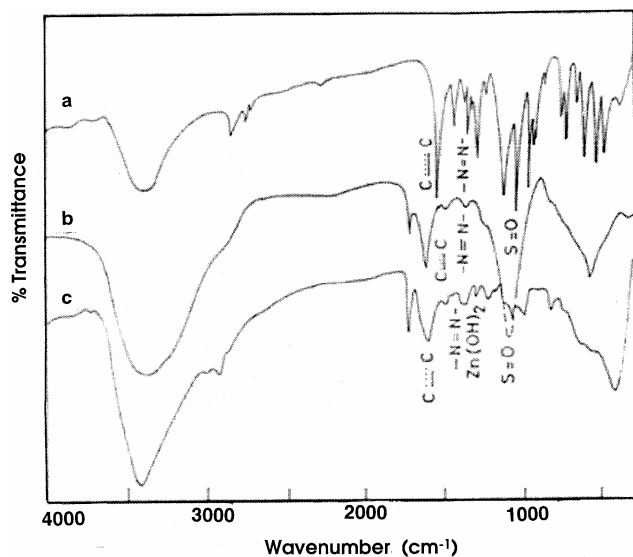


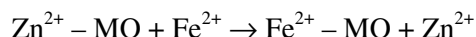
Fig. 3—FTIR Spectra of (a) Pure MO, (b) Prepared  $\text{Fe}^{2+}$ -MO complex, and (c) Film formed on the surface of carbon steel when immersed in 100 ppm MO + 50ppm  $\text{Zn}^{2+}$  solution

The FTIR spectrum of the film formed on the surface of the carbon steel after immersion in solution containing MO (100 ppm) and  $\text{Zn}^{2+}$  (50 ppm) is shown in Fig. 3c. The  $-\text{S}=\text{O}$  symmetric stretching frequency has shifted from 1120 to 1113  $\text{cm}^{-1}$ . The  $-\text{N}=\text{N}-$  has shifted from 1421 to 1392  $\text{cm}^{-1}$ . The aromatic  $\text{C}=\text{C}$  ring stretching frequency has shifted from 1608 to 1628  $\text{cm}^{-1}$ . The  $\text{C}-\text{N}$  stretching frequency has shifted from 1367 to 1392  $\text{cm}^{-1}$ . Spectrum shown in Fig. 3b is almost identical with spectrum shown in Fig. 3c. This confirms that the complex formed on the carbon steel under this study is identical with the complex prepared. The peak at 1350  $\text{cm}^{-1}$  is due to zinc hydroxide<sup>27,28</sup>.

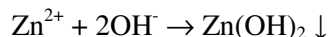
#### Mechanism of corrosion inhibition

In view of the above results, the following mechanism may be proposed for the corrosion inhibition of carbon steel immersed in well water:

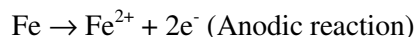
- (i) The formulation consisting of 100 ppm of MO and 50 ppm of  $\text{Zn}^{2+}$  in well water contains  $\text{MO}-\text{Zn}^{2+}$  complex in solution.
- (ii) When carbon steel is immersed in this solution  $\text{MO}-\text{Zn}^{2+}$  complex diffuses from the bulk of the solution to the metal surface.
- (iii)  $\text{MO}-\text{Zn}^{2+}$  complex is converted into  $\text{MO}-\text{Fe}^{2+}$  complex (as it is more stable than  $\text{MO}-\text{Zn}^{2+}$  complex) on the anodic sites of the metal surface with the release of zinc ion.



- (iv) The released  $\text{Zn}^{2+}$  combines with  $\text{OH}^-$  to form  $\text{Zn}(\text{OH})_2$  on the cathodic sites of the metal surface.



- (v) Thus, the protective film consists of  $\text{MO}-\text{Fe}^{2+}$  complex and  $\text{Zn}(\text{OH})_2$ .
- (vi) In near neutral aqueous solution, the anodic reaction is the formation of  $\text{Fe}^{2+}$ . This anodic reaction is controlled by the formation of  $\text{MO}-\text{Fe}^{2+}$  complex on the anodic site of the metal surface. The cathodic reaction is the generation of  $\text{OH}^-$ , which is controlled by the formation of  $\text{Zn}(\text{OH})_2$  on the cathodic sites of the metal surface.



This accounts for the synergistic effect of  $\text{MO}-\text{Zn}^{2+}$  system.

#### Conclusion

Methyl orange along with  $\text{Zn}^{2+}$  acts as a corrosion inhibitor system for carbon steel in well water. Its efficiency increased due to the transporting ability of zinc ion through the formation of the  $\text{MO}-\text{Zn}^{2+}$  complex. The IE of 100 ppm MO + 50 ppm  $\text{Zn}^{2+}$  system is found to decrease as the immersion period increases. A suitable mechanism has been proposed for the corrosion inhibition based on the results of polarization study and FTIR spectra. The protective film consists of  $\text{Fe}^{2+}$ -MO complex formed on the anodic sites and  $\text{Zn}(\text{OH})_2$  on the cathodic sites of the metal surface. This confirms that  $\text{MO}-\text{Zn}^{2+}$  system functions as a mixed inhibitor system.

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